

Variational Methods in the pursuit of an Action Principle in Fluid Turbulence

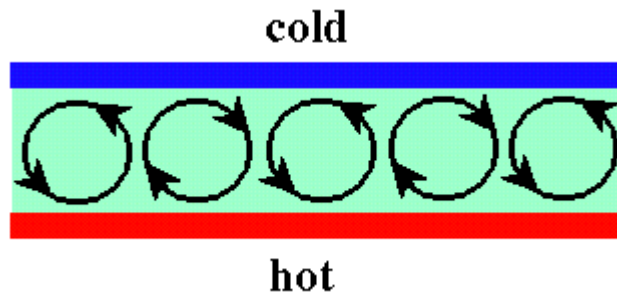
Rich Kerswell

Mathematics

Bristol University

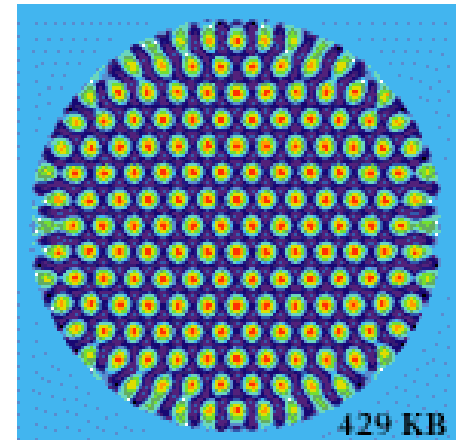
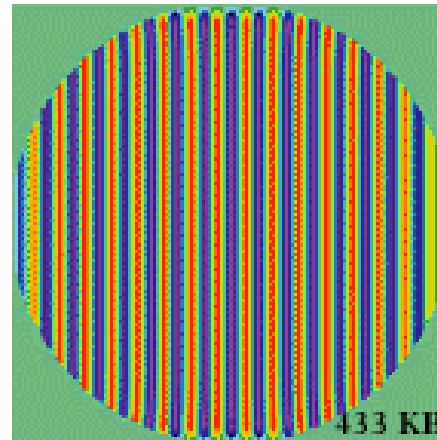
- Malkus' original idea - Maximum Entropy Production
- Variational Techniques
 - a) Euler-Lagrange (Howard-Busse)
 - b) Background approach (Doering-Constantin)
- "Efficiency" functional

Rayleigh-Benard convection

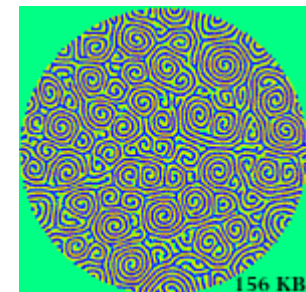
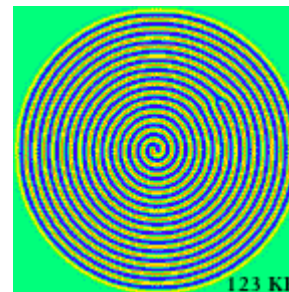


Malkus (1954a,b)

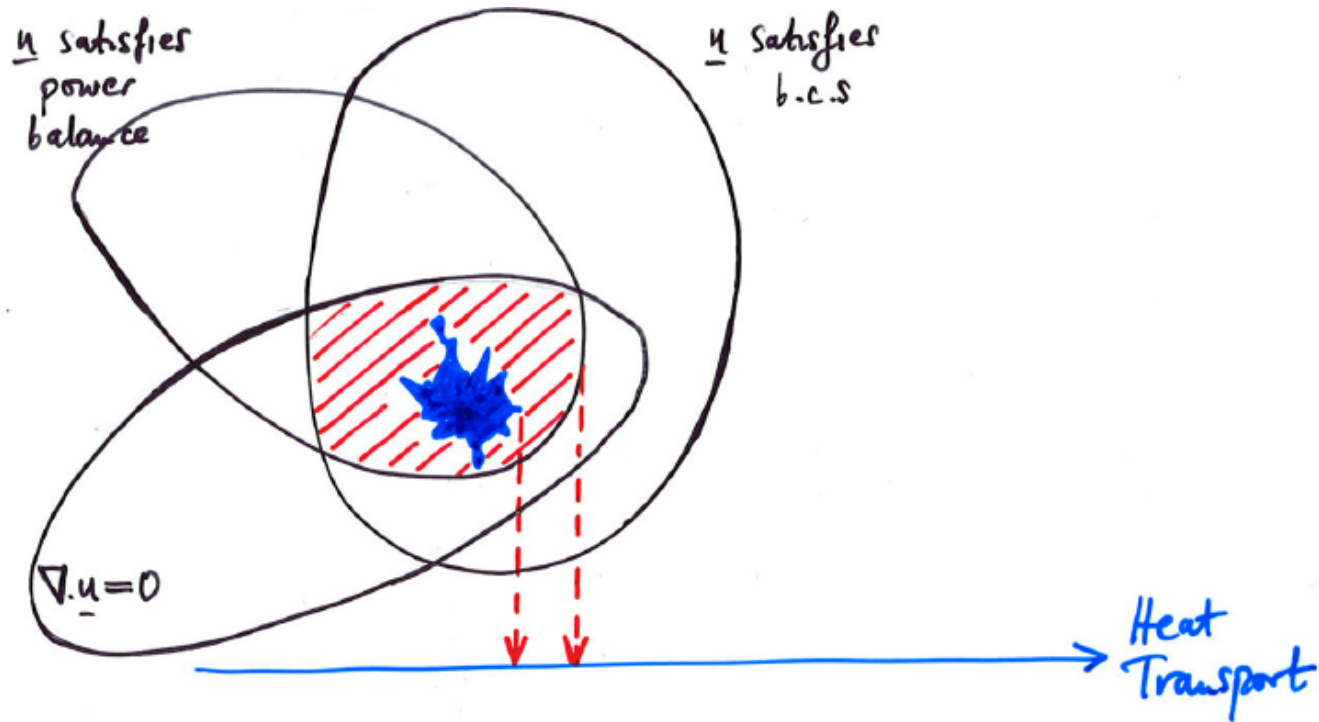
“Of all the possible solutions, the one which is selected is that which has the largest heat transport”



Malkus & Veronis (1958)



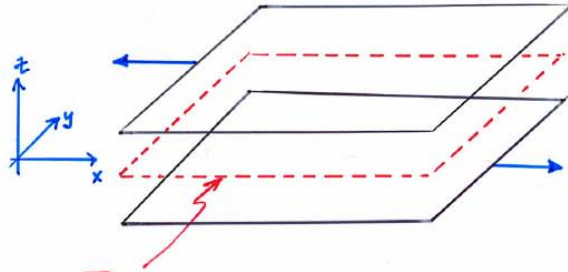
Extend competition to non-solutions - Howard (1963)



- strict upper bound
- applicable to turbulence

Classical Variational Approach

Busse (1970)



$$\frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u} + \nabla p = \nabla^2 \underline{u}$$

$$\nabla \cdot \underline{u} = 0$$

$$\underline{u} = \pm \frac{1}{2} \text{Re} \hat{\underline{x}} \quad z = \mp \frac{1}{2}$$

$$\text{Re} := \frac{V_0 d}{\nu}$$

$\overline{(\quad)} \equiv$ averaging over z planes

$\langle \quad \rangle \equiv \int dV$

Assumptions • $\underline{u}(x,t) = U(z)\hat{\underline{x}} + \underline{v}(x,t)$ with $\overline{\underline{v}} = \underline{0}$ so $\frac{\partial}{\partial t} \overline{\underline{u}} = \underline{0}$

• $\frac{d}{dt} \langle \frac{1}{2} \underline{v}^2 \rangle = 0$ on 'average' - statistical stationarity

Problem maximize $D = \int |\nabla \underline{u}|^2 dV$

subject to

i) total power balance $\int \underline{u} \cdot \left[\frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u} + \nabla p - \nabla^2 \underline{u} \right] d\underline{x} = 0$
 $\Rightarrow \langle U'^2 + |\nabla \times \underline{v}|^2 \rangle = -\text{Re} \frac{dU}{dz} \Big|_{\pm \frac{1}{2}} = \text{Re}^2 + \text{Re} \langle uw \rangle$

ii) mean momentum balance
 in $\hat{\underline{x}}$ direction $\lim_{L \rightarrow \infty} \frac{1}{4L^2} \int_{-L}^L dx \int_{-L}^L dy \hat{\underline{x}} \cdot \left[\frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u} + \nabla p - \nabla^2 \underline{u} \right] = 0$
 $\Rightarrow \frac{dU}{dz} = \overline{uw} - \langle uw \rangle - \text{Re}$

iii) flow incompressible $\nabla \cdot \underline{u} = 0$

iv) \underline{u} satisfies b.c.s $\underline{u}(x,y, \pm \frac{1}{2}) = \pm \frac{1}{2} \text{Re} \hat{\underline{x}}$

Euler-Lagrange Eqn

$$\Rightarrow \left[\overline{uw} - \langle uw \rangle - \frac{\text{Re}}{2} - \frac{\langle (\overline{uw} - \langle uw \rangle)^2 \rangle}{2 \langle uw \rangle} \right] \begin{bmatrix} w \\ 0 \\ u \end{bmatrix} + \nabla p = \nabla^2 \underline{v}$$

$$\nabla \cdot \underline{v} = 0$$

$$\underline{v}(x,y, \pm \frac{1}{2}) = 0$$

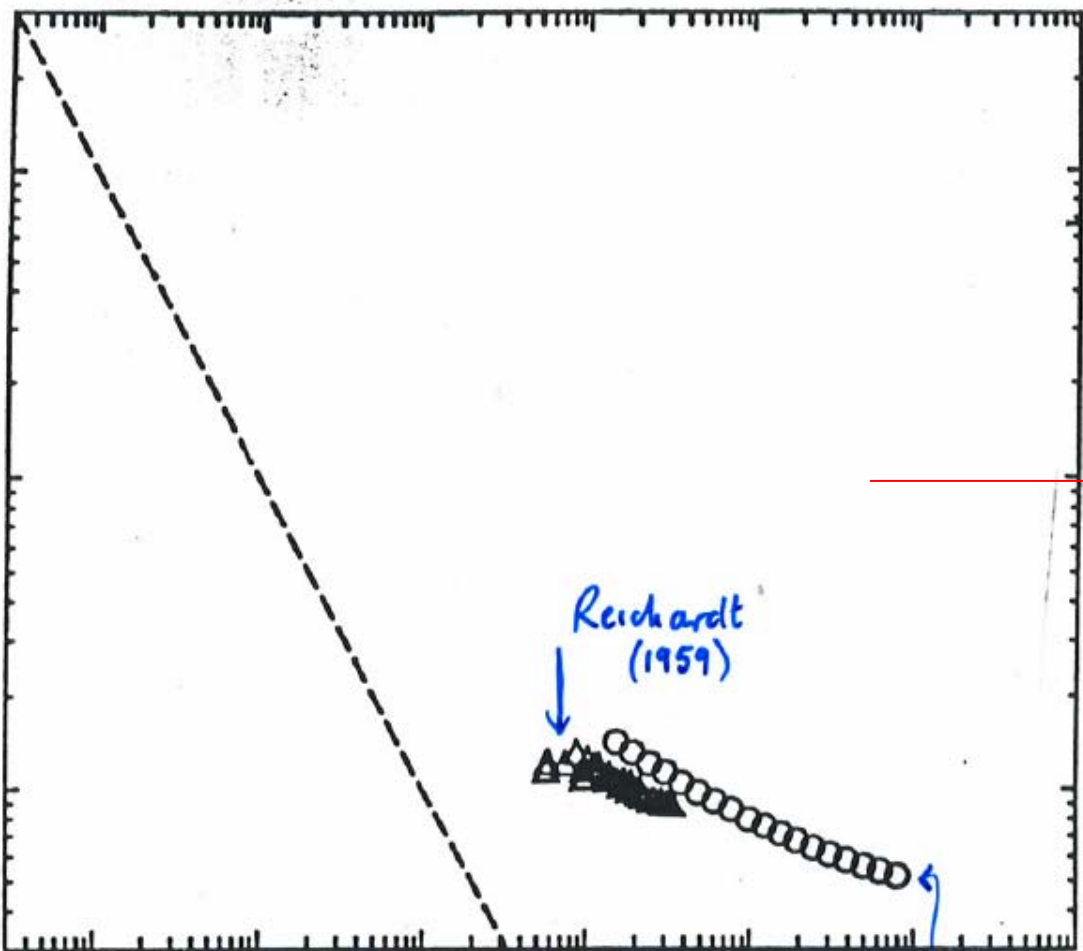
$$\frac{\varepsilon}{v^3/d}$$

0.100

C_ω

0.010

0.001



Reichardt
(1959)

Lathrop et al. (1992)

Re

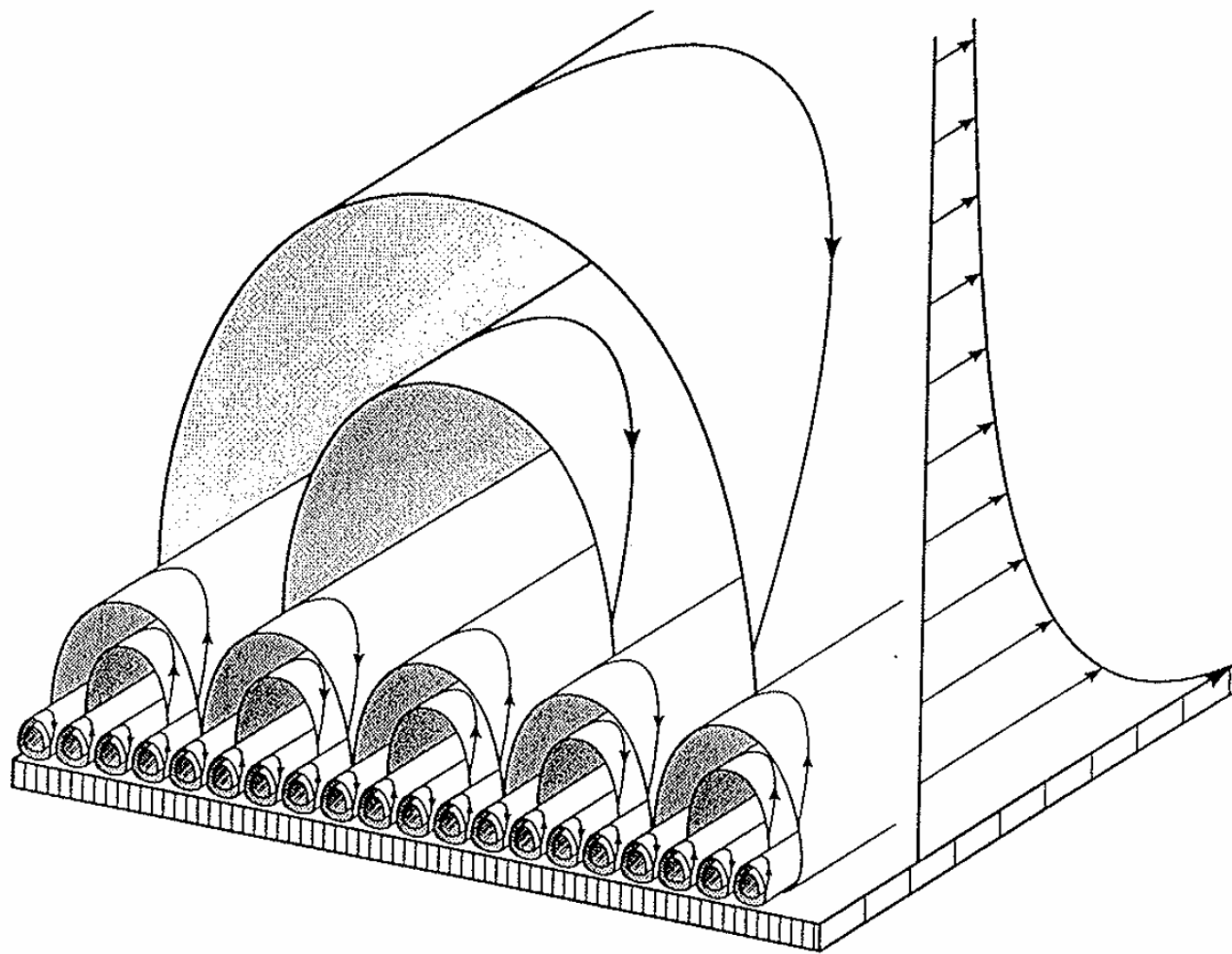


Fig. 1. Qualitative sketch of the nested boundary layers which characterize the vector field of maximum transport.

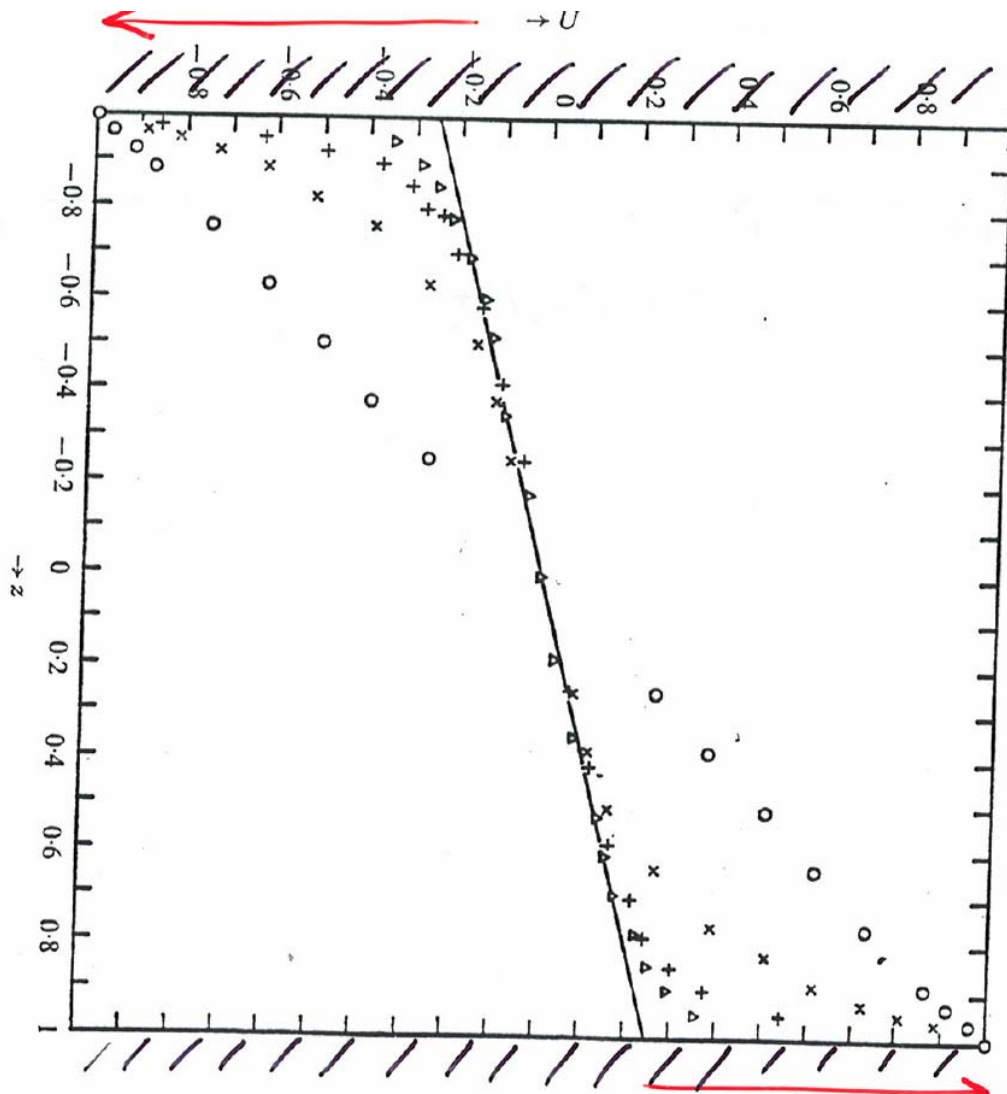


FIGURE 2. The mean velocity in plane Couette flow measured by Reichardt (1959) at $Re = 1200$ (\circ), $Re = 2900$ (\times), $Re = 5900$ ($+$), and $Re = 34000$ (Δ). The straight line describes the asymptotic profile corresponding to the extremalizing solution of the variational problem.

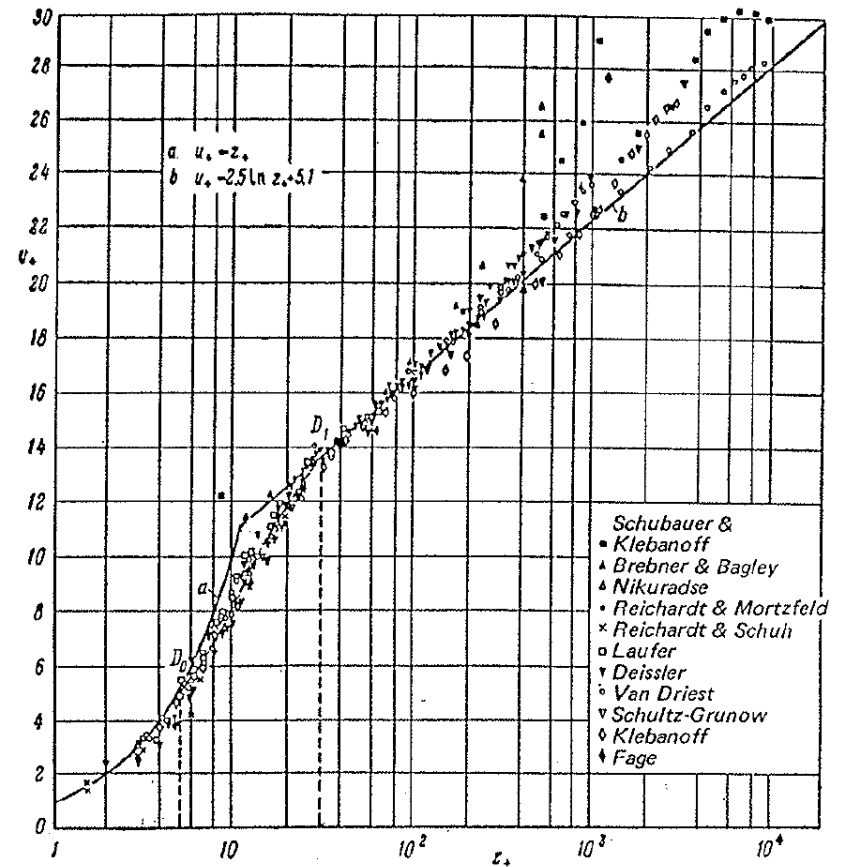
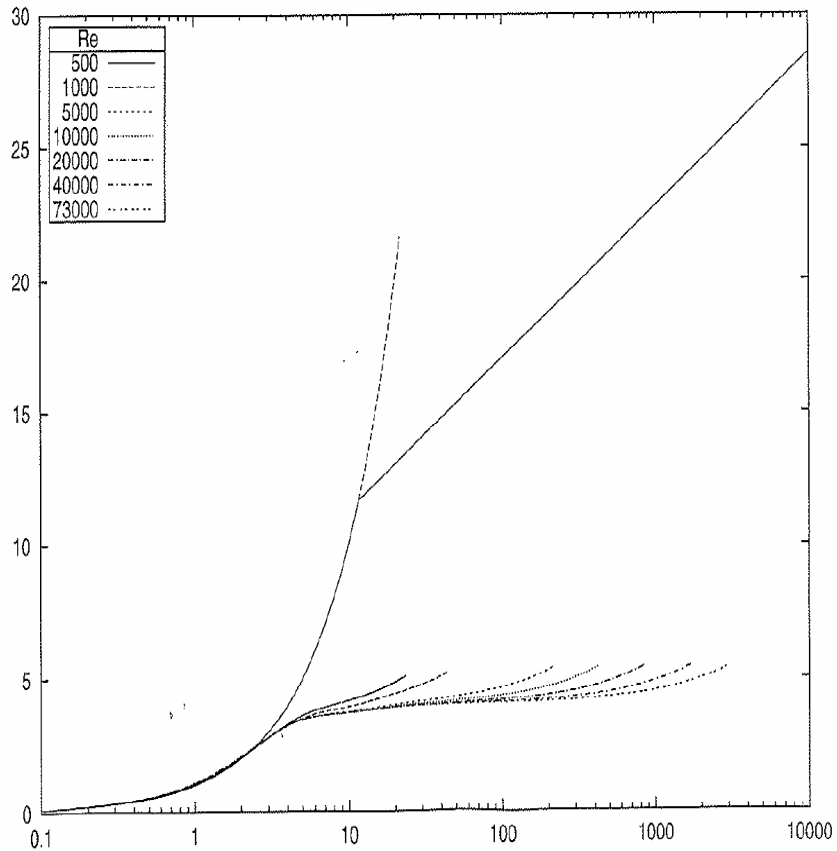


FIG. 25. Universal dimensionless mean velocity profile of turbulent flow close to a smooth wall according to the data of tube-, channel- and boundary-layer measurements [according to Kestin and Richardson (1963)].

Doering & Constantin (1992, 1994, 1995, 1996)
(Nicolis et al. 1997)

$$\underline{u}(\underline{x}, t) = \phi(\underline{z}) \hat{\underline{x}} + \underline{v}(\underline{x}, t)$$

(Hopf 1941)

⚡
 'Background' field
 $\phi(\pm \frac{1}{2}) = \mp \frac{1}{2} Re$

⚡
 'Fluctuations'
 $\underline{v} = 0|_{\partial \mathcal{D}}; \bar{\underline{v}} \neq 0$

Physical Information

$$\int_{\mathcal{D}} \underline{v} \cdot \left[\frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u} + \nabla p - \nabla^2 \underline{u} \right] d\underline{x} = 0$$

$$\Rightarrow \underline{\int} \frac{\partial}{\partial t} \int \frac{1}{2} \underline{v}^2 d\underline{x} = \int \phi'' v_1 - |\nabla \underline{v}|^2 - \phi' v_1 v_3 d\underline{x} \quad (\text{I})$$

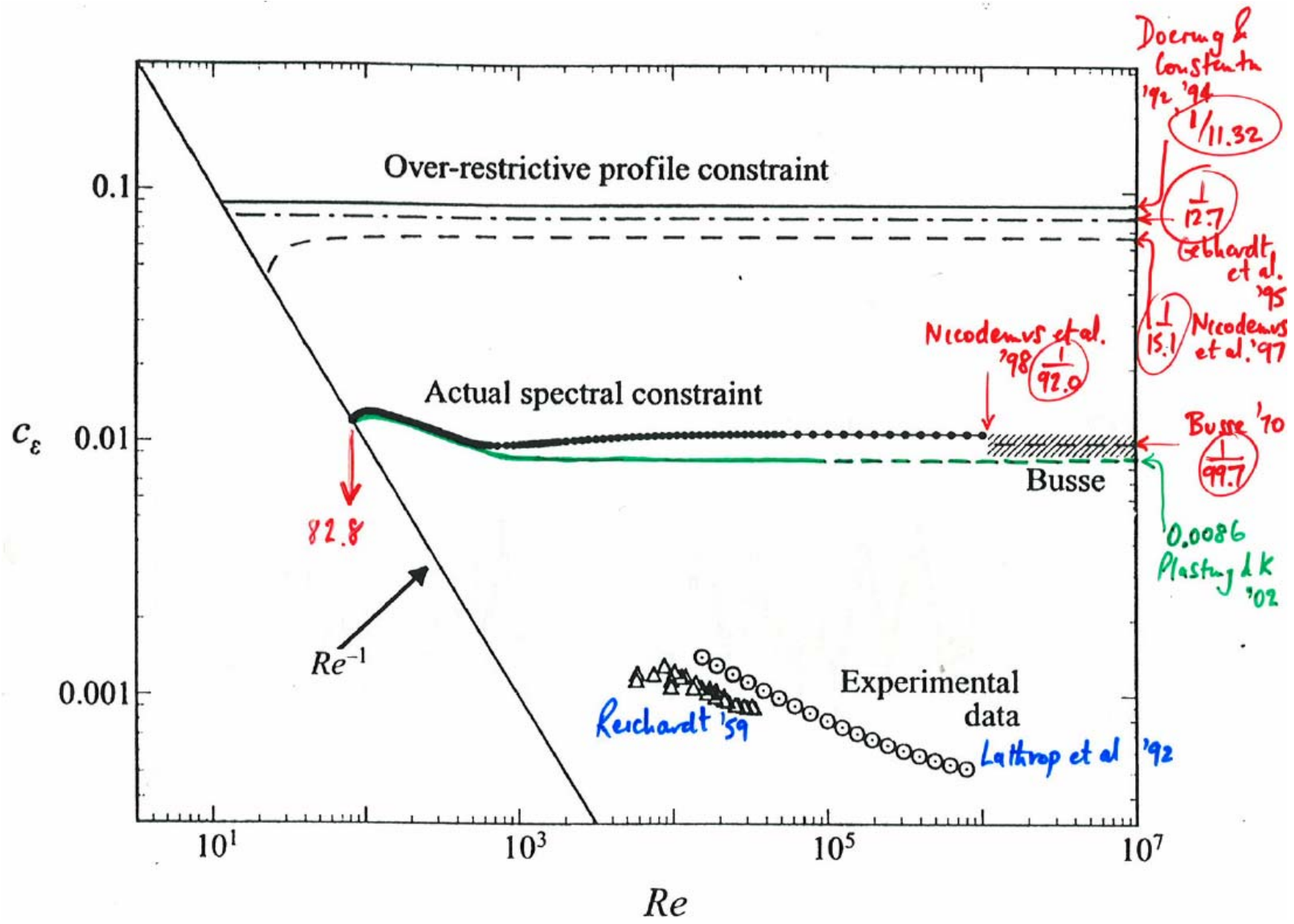
Identity $Re^3 \mathcal{D} = \int |\nabla \underline{u}|^2 d\underline{x} = \int |\phi' \hat{\underline{x}} + \nabla \underline{v}|^2 d\underline{x}$
 $= \int \phi'^2 - 2\phi'' v_1 + |\nabla \underline{v}|^2 d\underline{x} \quad (\text{II})$

$$(\text{II}) + a(\text{I}) \Rightarrow$$

$$Re^3 \mathcal{D} + a \frac{\partial}{\partial t} \int \frac{1}{2} \underline{v}^2 d\underline{x} = \int \phi'^2 - 2\phi'' v_1 + |\nabla \underline{v}|^2 + a\phi'' v_1 - a|\nabla \underline{v}|^2 - a\phi' v_1 v_3 d\underline{x}$$

Take long time averages $\left(\lim_{T \rightarrow \infty} \frac{1}{T} \int_0^T \frac{\partial}{\partial t} \int \frac{1}{2} \underline{v}^2 d\underline{x} dt = 0 \right)$

$$\lim_{T \rightarrow \infty} \frac{1}{T} \int_0^T Re^3 \mathcal{D} dt = \int \phi'^2 d\underline{x} - \lim_{T \rightarrow \infty} \frac{1}{T} \int_0^T dt \int (a-1) |\nabla \underline{v}|^2 + a\phi' v_1 v_3 - (a-2) \phi'' v_1 d\underline{x}$$



$$\max/\min u^2 \quad \text{s.t. } u=1$$

$$\mathcal{L} = u^2 - av(u-1)$$

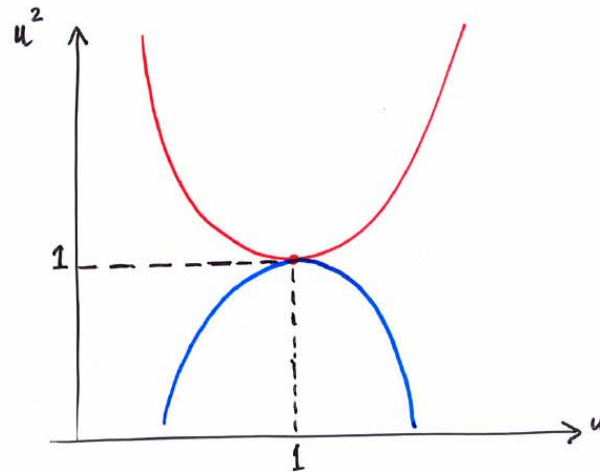
define $\phi = u - v$

$$\Rightarrow \mathcal{L} = \phi^2 + (2-a)v\phi - (a-1)v^2 + av$$

$$(a) \quad \left. \frac{\partial \mathcal{L}}{\partial v} \right|_{\phi} = 0 \Rightarrow v = \frac{(2-a)\phi + a}{2(a-1)}$$

$$\Rightarrow \mathcal{L} = 1 + \left[\frac{a\phi + (2-a)}{4(a-1)} \right]^2$$

MINIMIZATION problem over ϕ (D-C)



$$(b) \quad \left. \frac{\partial \mathcal{L}}{\partial \phi} \right|_v = 0 \Rightarrow \phi = \left(\frac{a-2}{2} \right) v$$

$$\Rightarrow \mathcal{L} = 1 - \left(\frac{a}{2} v - 1 \right)^2$$

MAXIMIZATION problem over v (B)

Stability of the Mean Profile?

parametrization of data (Reynolds & Tiederman 1967)

$$U(y) = RB \int_0^y \frac{1-y'}{1+E(y')} dy', \quad (3.1)$$

where $R = \frac{\langle U \rangle y_0}{\nu}$, $B = -\frac{\partial P}{\partial x}(y=0)$, $\int_0^1 U dy = 1$, (3.2)

and $E(y) = \frac{1}{2} \left\{ 1 + \frac{K^2 R^2 B}{9} (2y-y^2)^2 (3-4y+2y^2)^2 \left(1 - \exp\left(\frac{-yRB^{1/2}}{A}\right) \right)^2 \right\}^{-1/2}$. (3.3)

(A) Linear Stability of $U(y)$ Reynolds & Tiederman (1967)

$$Re^* \simeq 10 Re$$

(B) Linear Stability of $U(y) +$ Reynolds Stress component of OS mode

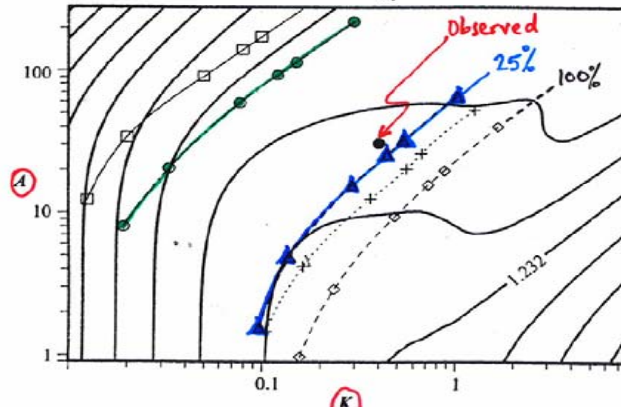
$$Re^* \simeq 5 Re$$

Ierley & Malkus (1988)

(C) Linear Stability of $U(y) \hat{x} + A^* \underline{u}_{os}^{2D}$ to 3D disturbances

$Re^* \sim Re$ if A^* such that u_{os}^{2D} peak speed is 25% local mean velocity

← that required to make mean inflexional
100% = 1% energy of mean

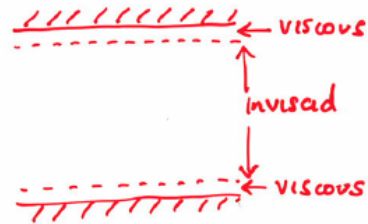


Alternative functionals

Mallus & Smith (1989) PPF

Smith (1991) PCF

Ierley & Worthing (2001) HPPF



'Approximate' Variational Problem

$$\max f = D \times I^n$$

$$I := \frac{D_{\text{fluctuation}}}{D_{\text{mean}}} = \frac{D_v}{D_m}$$

over all $u^+(z)$ where

a) smallest scale of motion in $u^+(z)$ is given by a critical boundary Reynolds number

b) 'interior' is inviscidly stable $u^{+''} < 0$

c) b.c.s implied on u^+ via mean momentum balance

$$u^{+''''} = u^+ = 0; \quad u^{+''} = R^*; \quad u^{+'} = \pm R^* \quad \text{at } z = \mp 1$$

$$u^{+''} = -I^* I \quad \text{where } I = \sum_0^{k_0} I_k e^{ik(1+z)\pi} \quad (\text{Fejér})$$

$n=1$ gives interesting results
christened $f = DI$ the "efficiency" functional

Efficiency
 $\xi_1 = \xi \left(\frac{\epsilon_{fluct}}{\epsilon_{mean}} \right)$

Bounds on functions of the dissipation rate

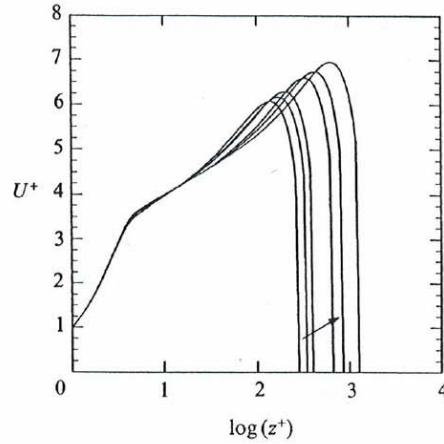


FIGURE 9. Maximum- ϵ profiles for $R = 738, 922, 1107$ (numerical) and $R = 1913, 2519, 3867$ (approximate). $k_0 = 89, 109, 128, 210, 270, 400$.

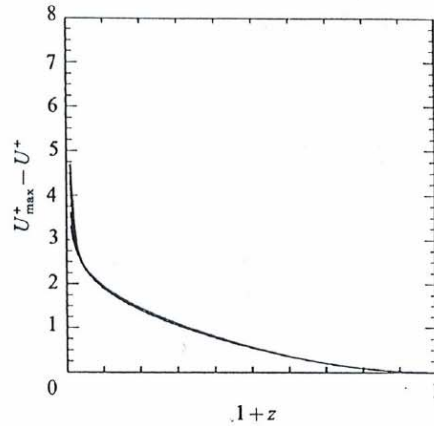
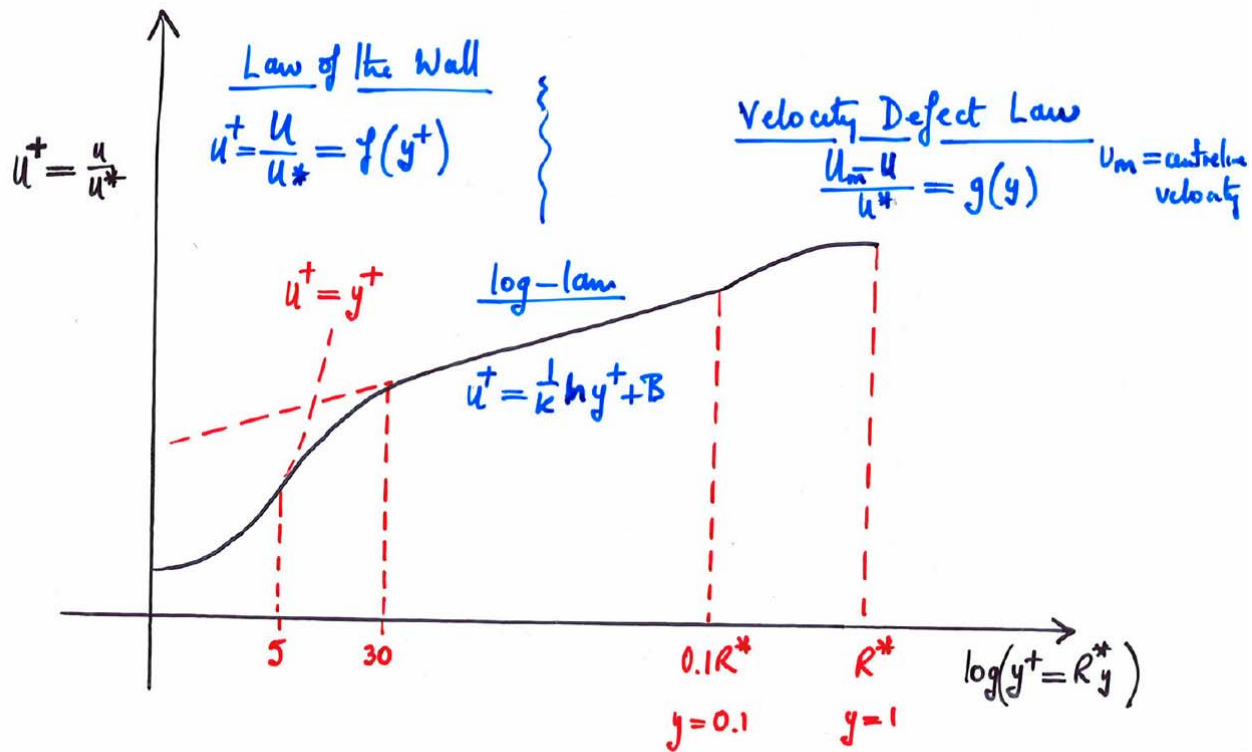
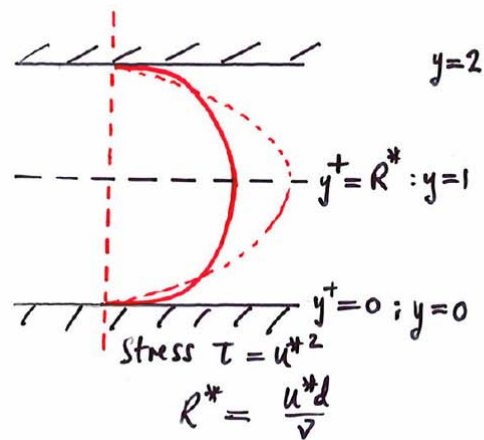


FIGURE 10. Maximum- ϵ velocity defect law of both the numerical and approximate profiles.

Malik & Smith (1989)

e.g. Plane Poiseuille Flow (PPF)



Bounds on functions of the dissipation rate

Mean Fields
data &
optimal roll!

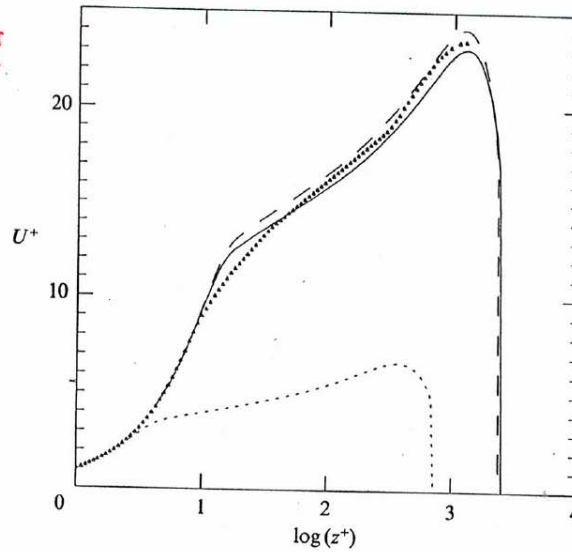


FIGURE 12. Recent experimental data for Poiseuille channel flow, and \mathcal{E} upper-bound profiles for different R_c . Δ , data (Johansson *et al.* 1983), for $R \approx 25\,600$; —, maximum- \mathcal{E} profile with $R_c = 480$ ($k_0 = 230$, $R \approx 25\,600$); —, maximum- \mathcal{E} profile with $R_c = 529$ ($k_0 = 210$, $R \approx 25\,600$); - - maximum- \mathcal{E} profile with $R_c = 39.69$ ($k_0 = 230$, $R \approx 2100$).

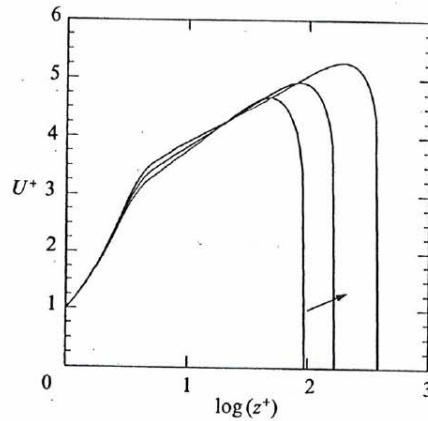


FIGURE 13. Maximum- $R^{5/2}I$ profiles for $R = 192, 369, 1107$ ($k_0 = 30, 53, 121$).

Apply variational machinery to "Efficiency" functional

$$J = DI^n \text{ \& \ } D_m I^n$$

in plane Couette flow (PCF)
 & plane Poiseuille flow (PPF) (K 2002)

Results

J		I	D	(PCF) interior shear
DI^n	$0 \leq n < 1$	$O(1)$	$O(Re^3)$	$-\left(\frac{3n+1}{4}\right)Re$
"efficiency"	$n=1$	$O(Re^{\frac{1}{3}})$	$O(Re^{\frac{8}{3}})$	$-Re$ (laminar)
	$n > 1$	$O(Re^{\frac{1}{2}})$	$O(Re^{\frac{3}{2}})$	$-Re$
D_m		$\frac{1}{2}$	$O(Re^3)$	0
Observed (Prandtl-von Kármán)		$O(\log Re)$	$O\left(\frac{Re^3}{(\log Re)^2}\right)$	0 (presumed as $Re \rightarrow \infty$)

- Efficiency does not give a log-layer & velocity defect law
- D_m gives correct interior for PCF
but incorrect for PPF
- "stability" missing!

Summary

Variational methods are a valuable tool

- Extract (inequality) scaling laws

e.g. wall-bounded shear flows $e \sim O(1)$ as $n \rightarrow 0$

Boussinesq convection $Nu \sim Ra^{1/2}$

- Test hypotheses

(a) effect of extra constraints...

(b) look for an Action functional

- Efficiency is promising but unsubstantiated

Key omissions are **Stability** constraints...

Theorem

In Plane Couette flow, for a velocity field which satisfies the Navier-Stokes equations & the smoothness constraint that the minimum lengthscale parallel to the plates $\geq \lambda Re^{2\alpha-1}$ then the energy dissipation rate $\varepsilon \leq \varepsilon_{\text{bound}}$ where

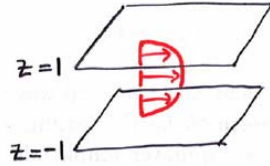
$$\frac{0.308}{\sqrt{\lambda}} Re^{-\alpha} \leq \varepsilon_{\text{bound}} \leq \frac{0.562}{\sqrt{\lambda}} Re^{-\alpha} \quad \text{as } Re \rightarrow \infty$$

(Kerswell 2000)

Implications

1. If $\varepsilon \sim O(1)$ (or there are logarithmic corrections)
 \Rightarrow transverse lengthscales down to $O(Re^{-1})$ are important
2. Numerical simulations which adopt, e.g., $|k|_{\text{max}} = \frac{2\pi}{\lambda_{\text{Kolmogorov}}}$
will manage at best $\varepsilon \sim Re^{-1/4}$
3. Suggest numerical experiments in which transverse scales are artificially restricted.

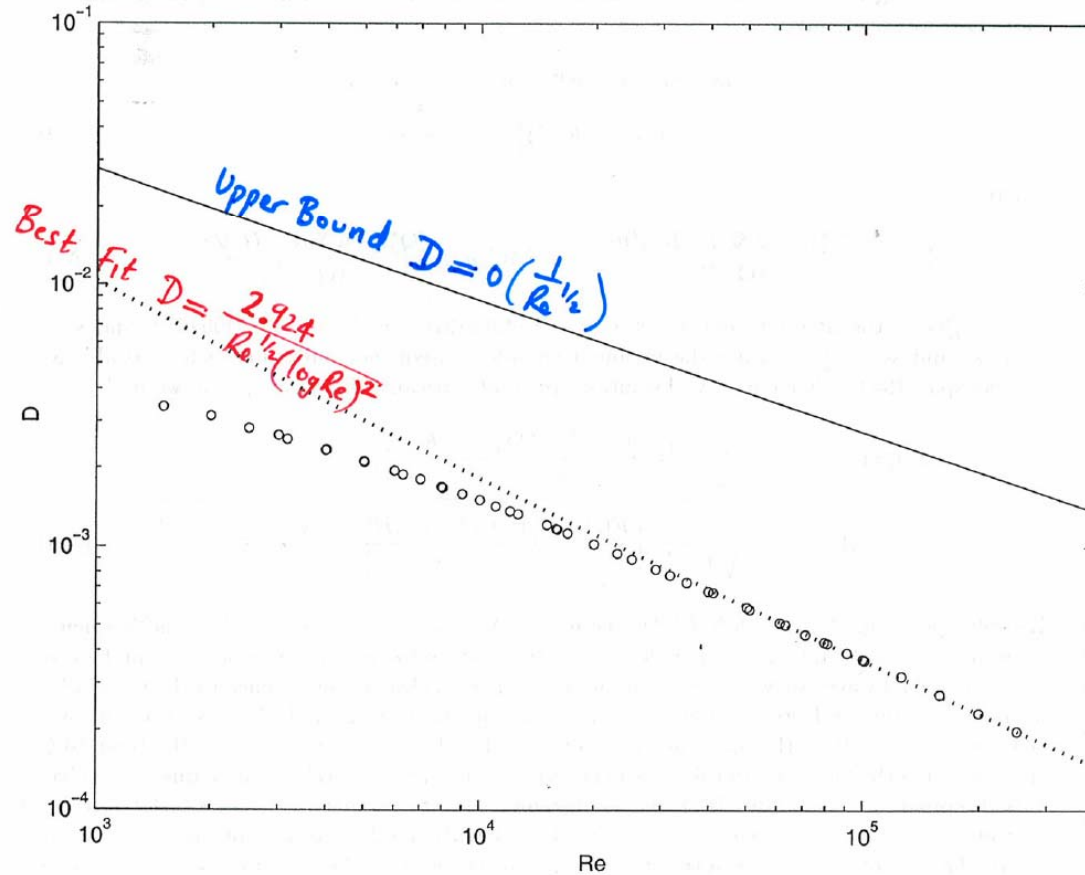
(PPF) Plane Poiseuille Flow



$$\underline{v} = \sum_{\underline{k}} \underline{v}_{\underline{k}}(z) e^{i \underline{k} \cdot \underline{x}}$$

$$\underline{k} = (k_1, k_2, 0)$$

$$-10 \leq k_1, k_2 \leq 10$$



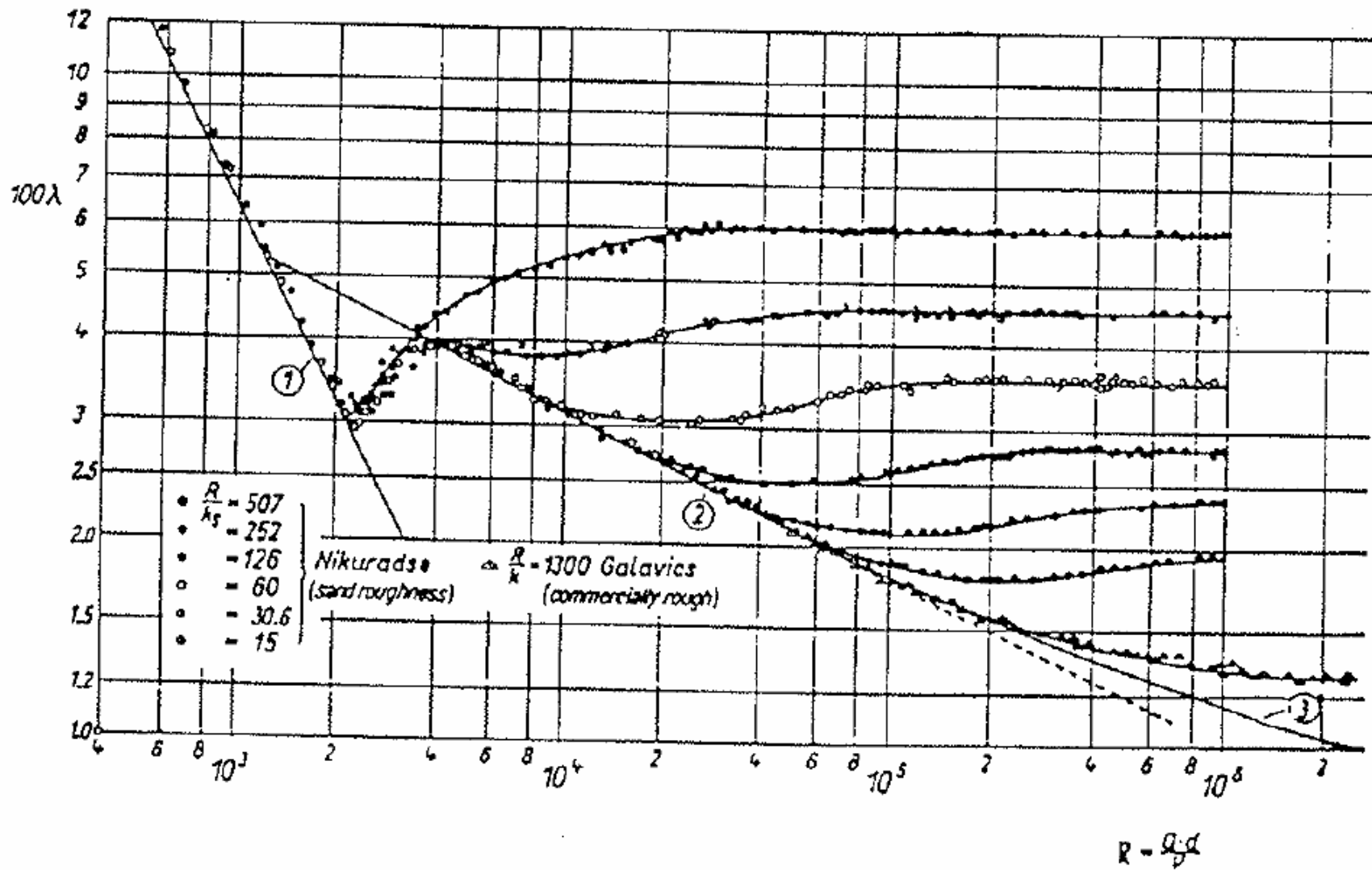


Fig. 20.18. Resistance formula for rough pipes

Curve (1) from eqn. (5.11), laminar; curve (2) from eqn. (20.5), turbulent, smooth; curve (3) from eqn. (20.30), turbulent, smooth

Worthing
(1995)

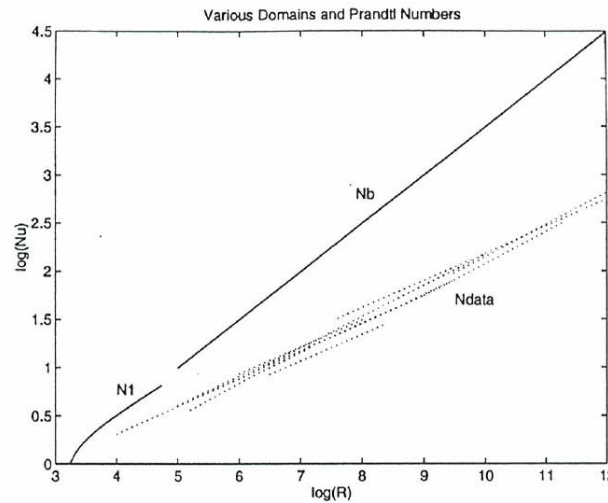


Figure 4-1: The Howard-Busse upper bound and experimental data.

- N1 Howard's single- α bound (computed here)
- Nb Busse's (1969) $R \rightarrow \infty$ infinite- α bound
- Ndata Various experimental data.

Sommeria (1999)

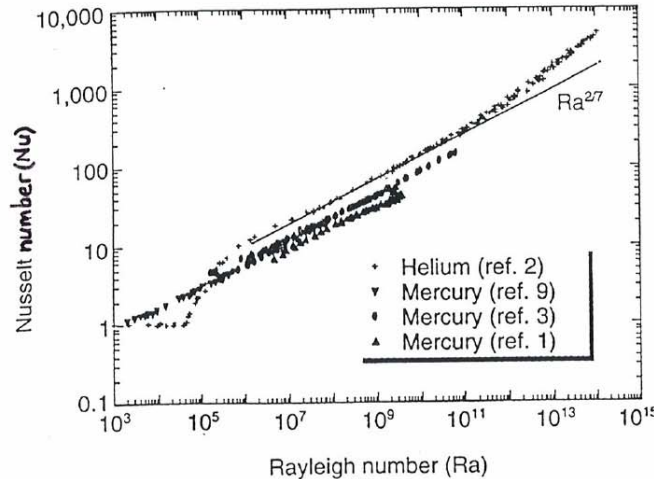
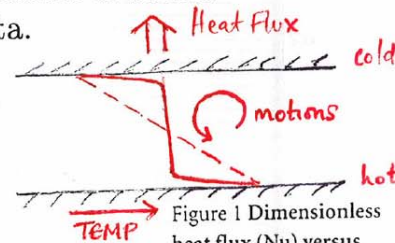


Figure 1 Dimensionless heat flux (Nu) versus temperature difference (Ra) in Rayleigh-Bénard convection. In mercury ($Pr = 0.025$), data from three experiments agree with the $Nu \propto Ra^{2/7}$ law^{1,3,9}. In helium ($Pr \approx 1$) the data² indicate an increase in Nu, and possibly a trend towards an ultimate regime, $Nu \propto Ra^{1/2}$. Although Ra is smaller in mercury than in helium, the corresponding Reynolds numbers are comparable.

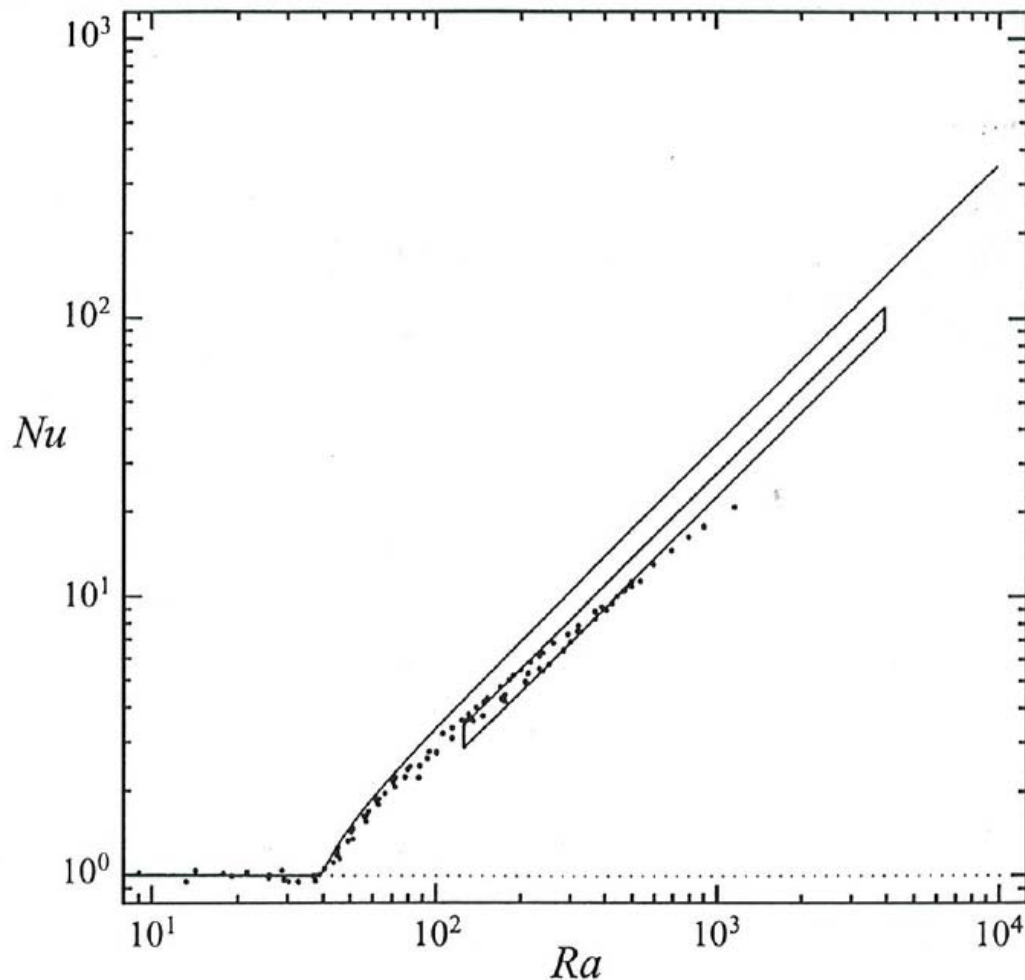
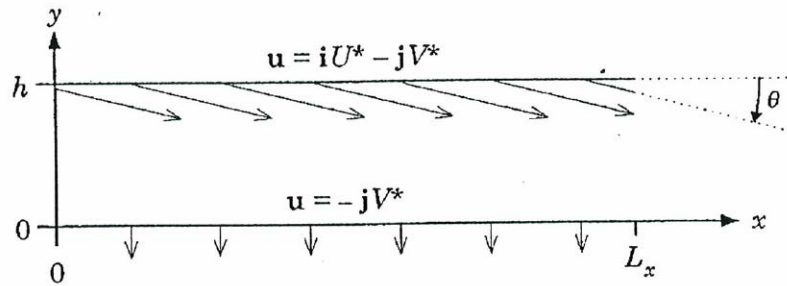


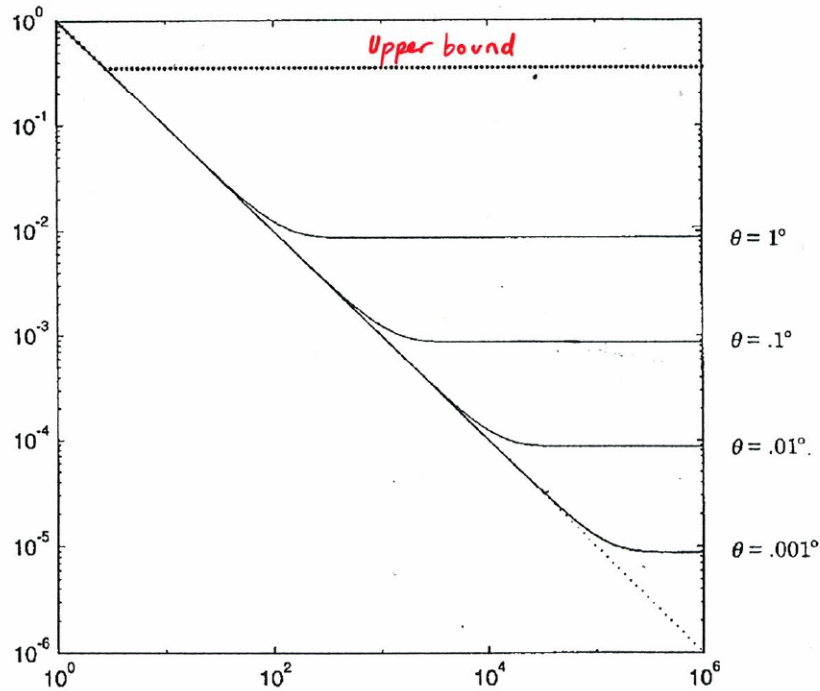
FIGURE 7. Rigorous upper bound plotted along with experimental data (see caption to Figure 6). The solid curve is the lower envelope of the curves in figure 6 for all $a \in (0, 1)$.

Couette Flow
with suction

Doering, Spiegel & Worthing (2000)



$D \left[\frac{u^*{}^3}{h} \right]$



laminar
dissipation

Re